



Consideration of Gas Hydrate Production Well Technology

August 17, 2005

**PRACTICAL SOLUTIONS
TO COMPLEX PROBLEMS**



Gas Hydrate Production Well Technology

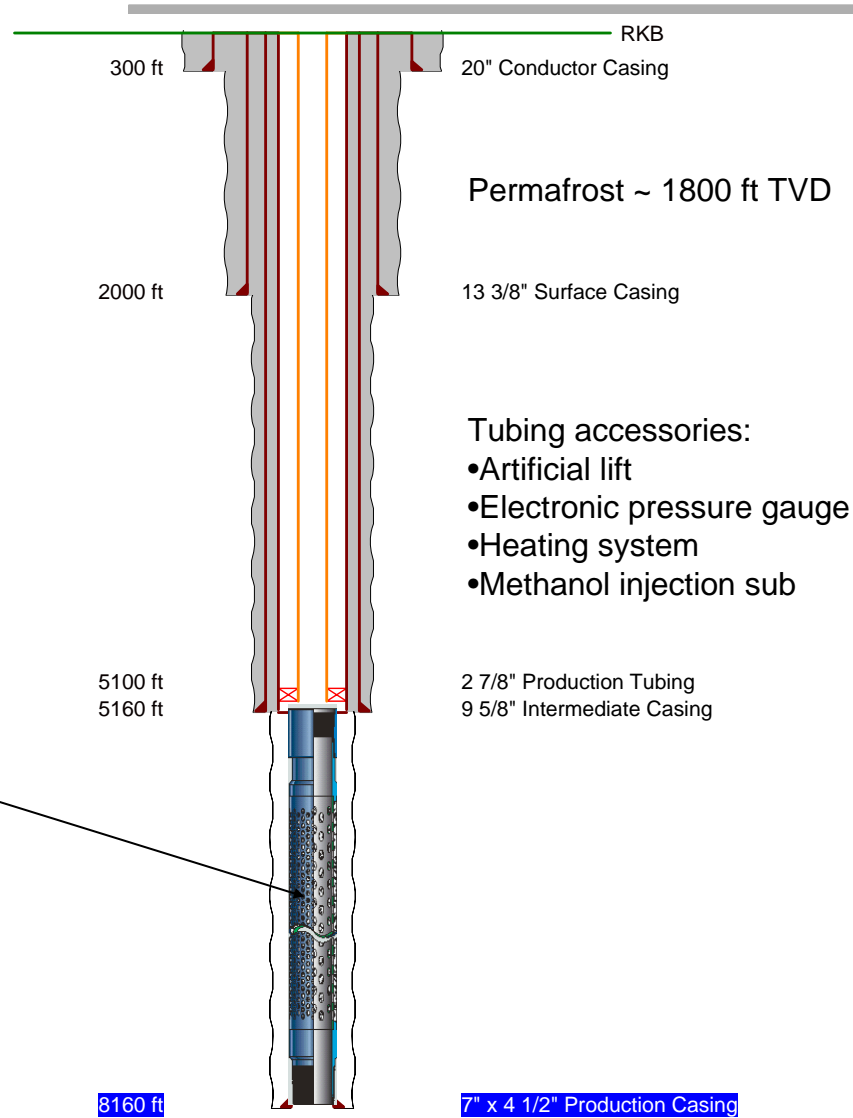
- Drilling & completion issues

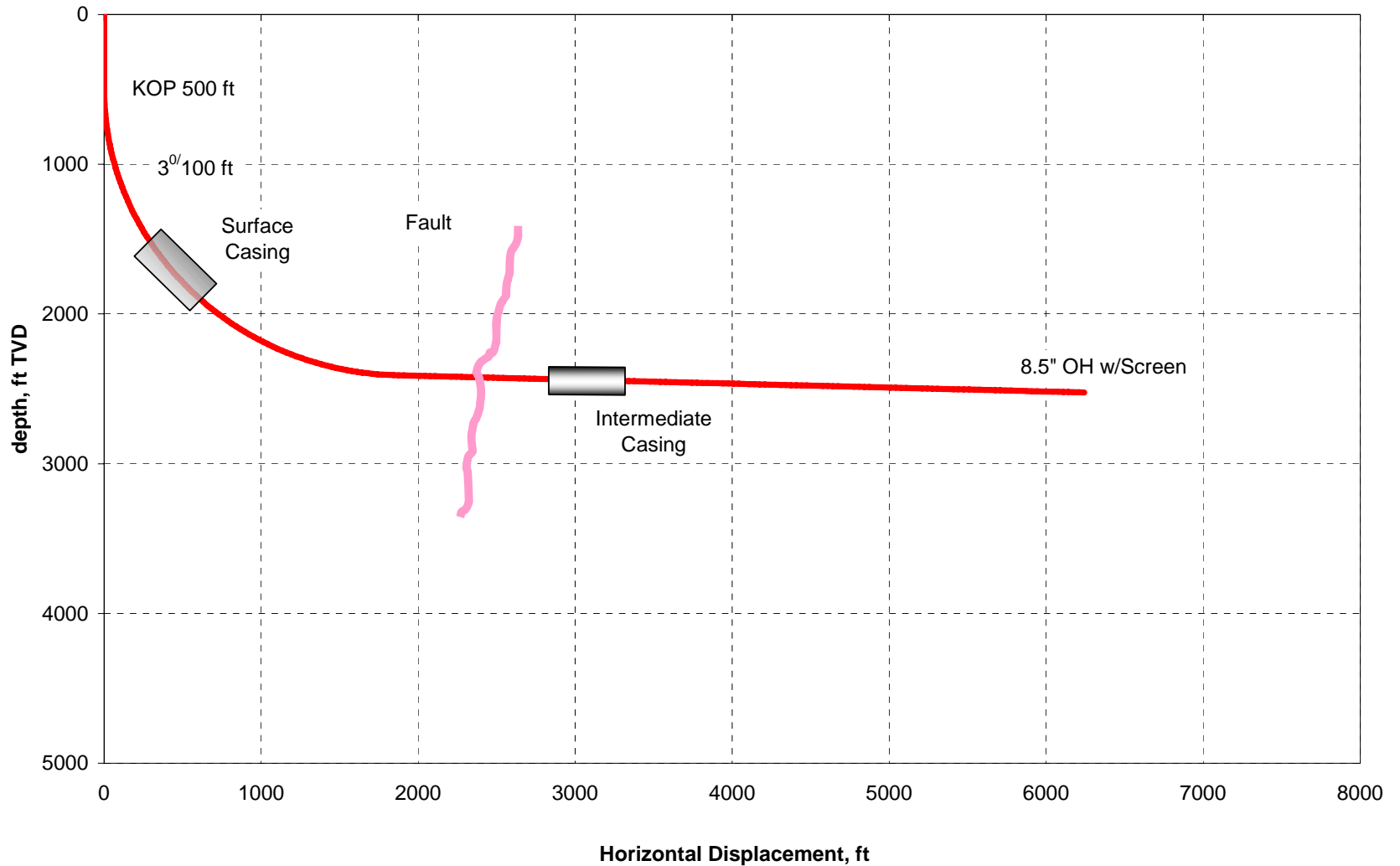
- Well performance issues
 - Flowing pressures
 - Water production
 - Other flow assurance issues

- Field development review based on Mallik

Typical Well Completion

Sand screen shroud will incorporate fibre optic loops with distributed temperature and several discrete pressure sensors





Conventional Gas Reservoir

- Typically normal or higher initial reservoir pressure
- FBHP controlled by:
 - Drawdown limitation (borehole stability, water production etc.)
 - Surface pressure constraint
 - Rate constraint
- Compression typically staged later in life of field

Gas Hydrate Reservoir

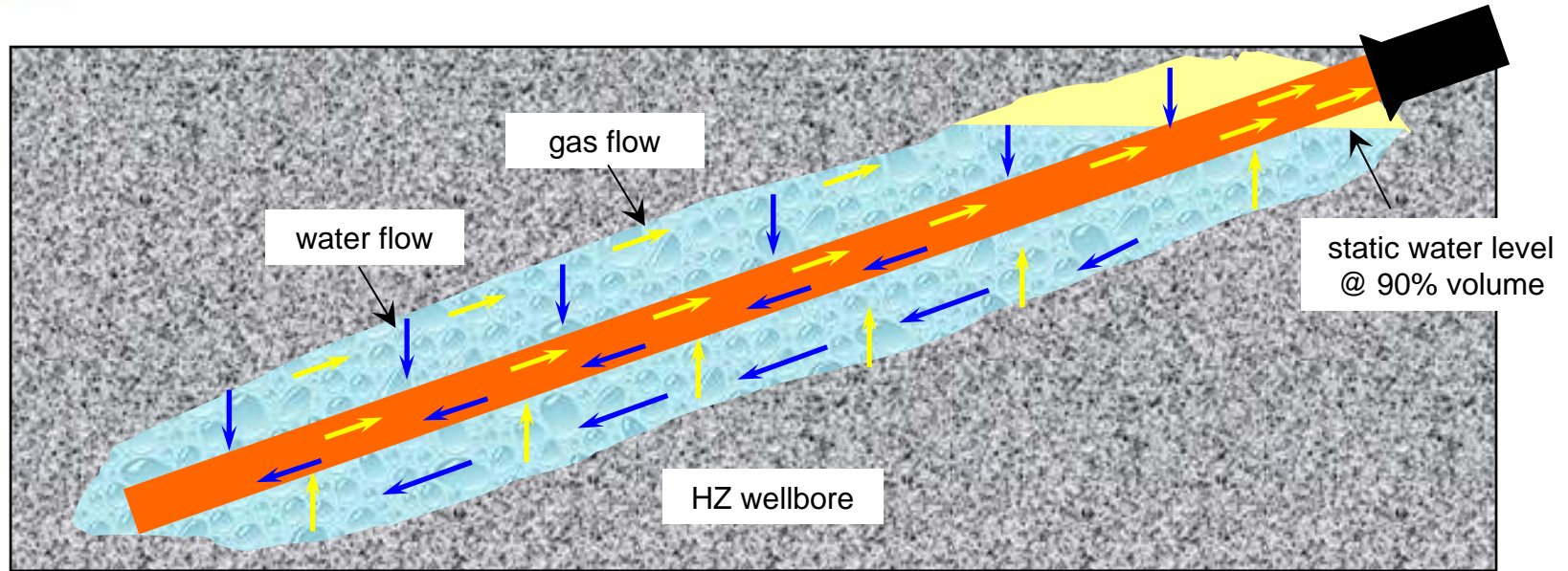
- Initially normally pressured (water phase pore pressure)
- FBHP controlled by dissociation (say 350-500 psi)
- Production rate must equal dissociation rate
- FWHP controlled by FBHP and production rate (gas & water)
- Compression required throughout life of project

Conventional Gas Reservoir

- Water sources:
 - 1-2 bbls/MMscf condensation
 - Coning & cusping
 - Active aquifer
- Historical controls (low cost):
 - Cyclic operation
 - FWHP reduction
 - Water shut-off re-completions
 - Lift assist
- Other controls (high cost):
 - Sidetrack/horizontal well
 - Artificial lift (gaslift, PD pumps, jet pumps)

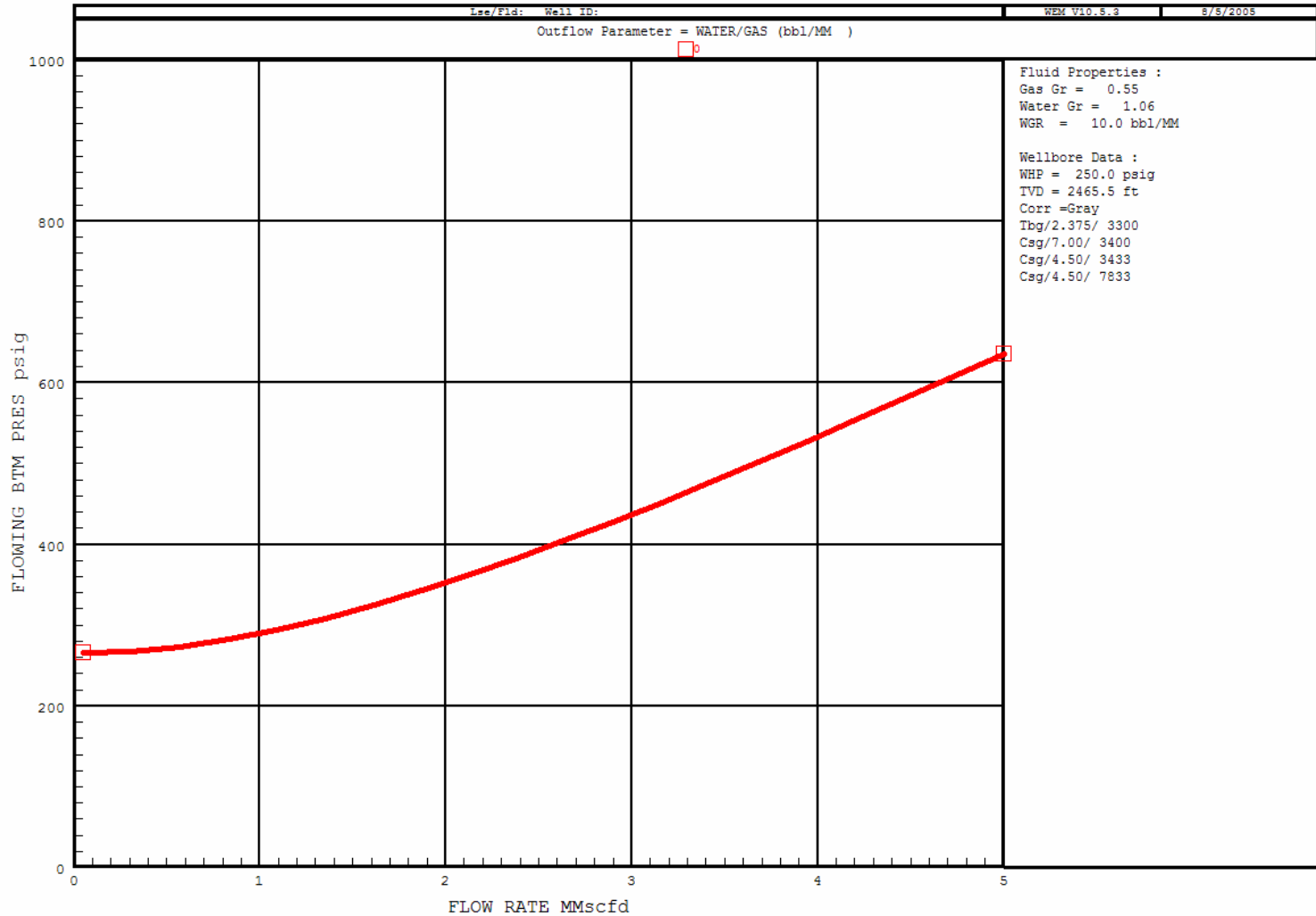
Gas Hydrate Reservoir

- 1 ft³ of gas hydrate = 164 scf of gas & 0.9 ft³ of water:
 - ~ 978 bbls/MMscf
 - Actual water production function of well geometry, reservoir drainage
- Low FBHP conditions provides stable tubing performance with relatively high watercuts
- Artificial lift required:
 - Well start-up
 - Continuous and/or intermittent basis
- Disposal or resource (low salinity)

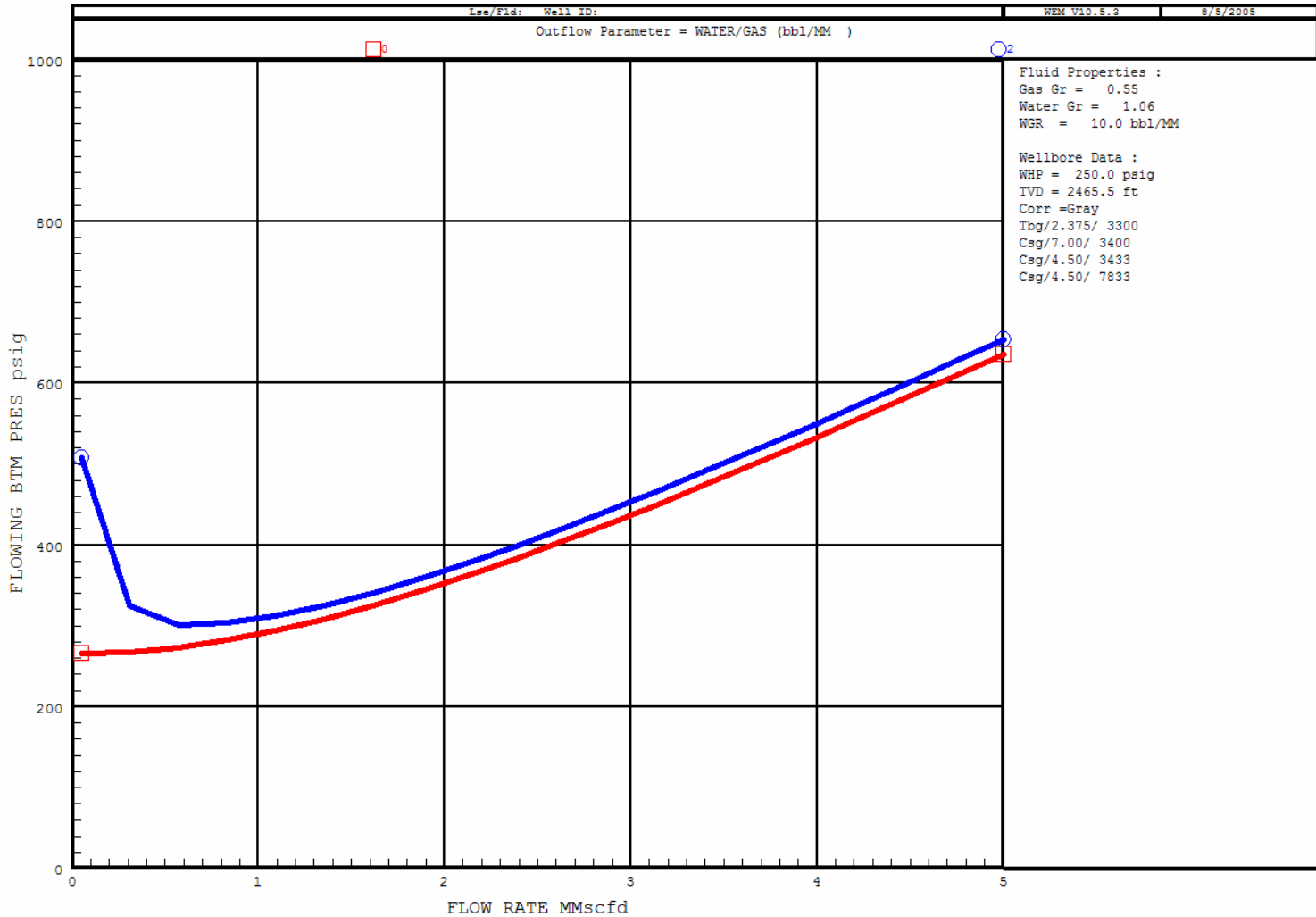


- No Free water
- Gravity effect dominate gas/water segregation
- Gas will accumulate along top of dissociated zone, expansion due to low pressure will drive gas towards wellbore
- No driving energy in free water phase – gas velocity only???

2 3/8" Tubing Performance

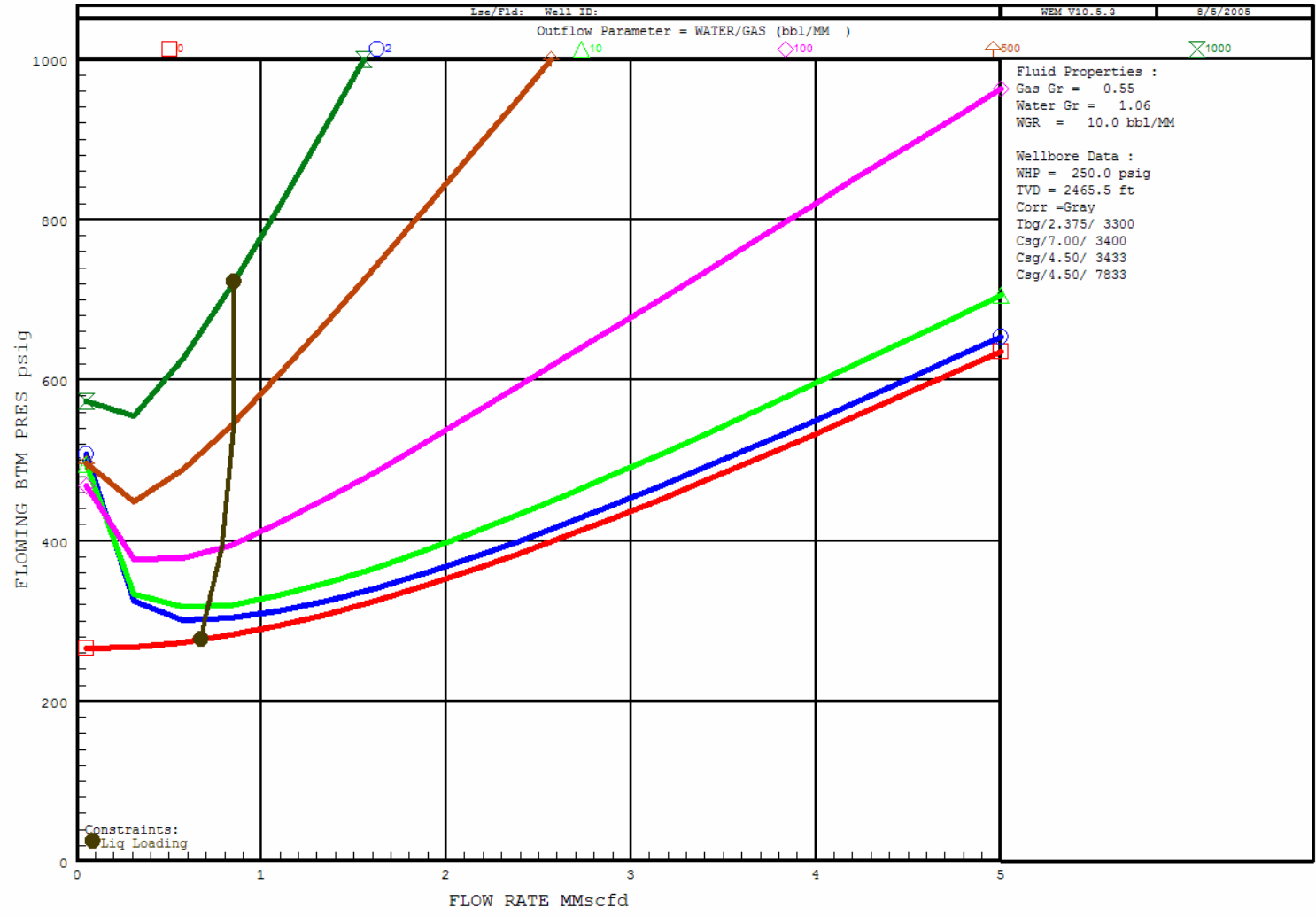


2 3/8" Tubing Performance





2 3/8" Tubing Performance



Conventional Gas Reservoir

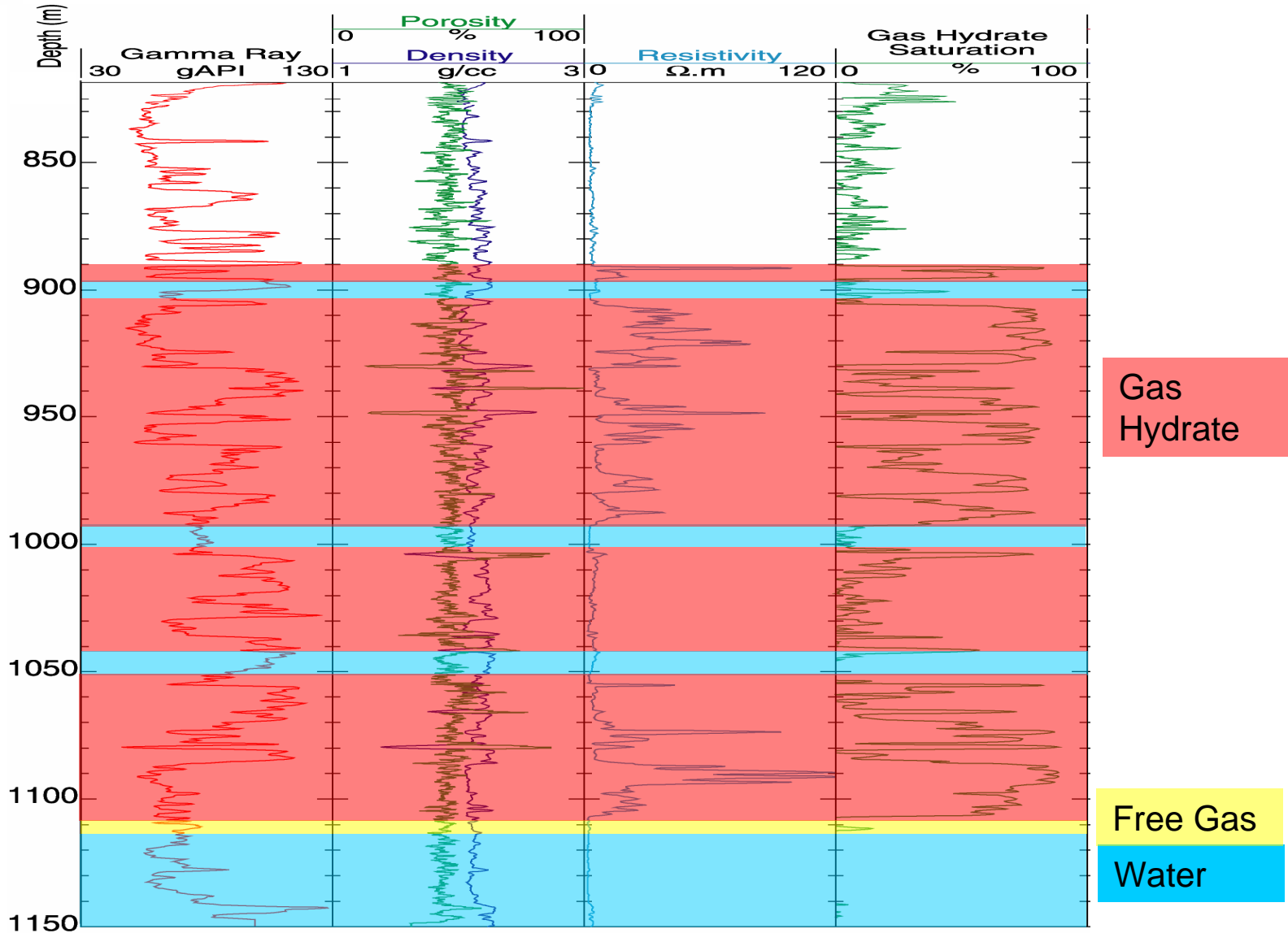
- Hydrate formation prevention:
 - FWHT > 75 F depending upon gas analyses & pressure
 - Temporary heating or chemical injection
- Liquid loading
- Others:
 - CO₂ & H₂S (corrosion)
 - Scale (produced water)
 - Asphaltenes & paraffins (gas condensate)
 - Extreme high temperatures and pressures

Gas Hydrate Reservoir

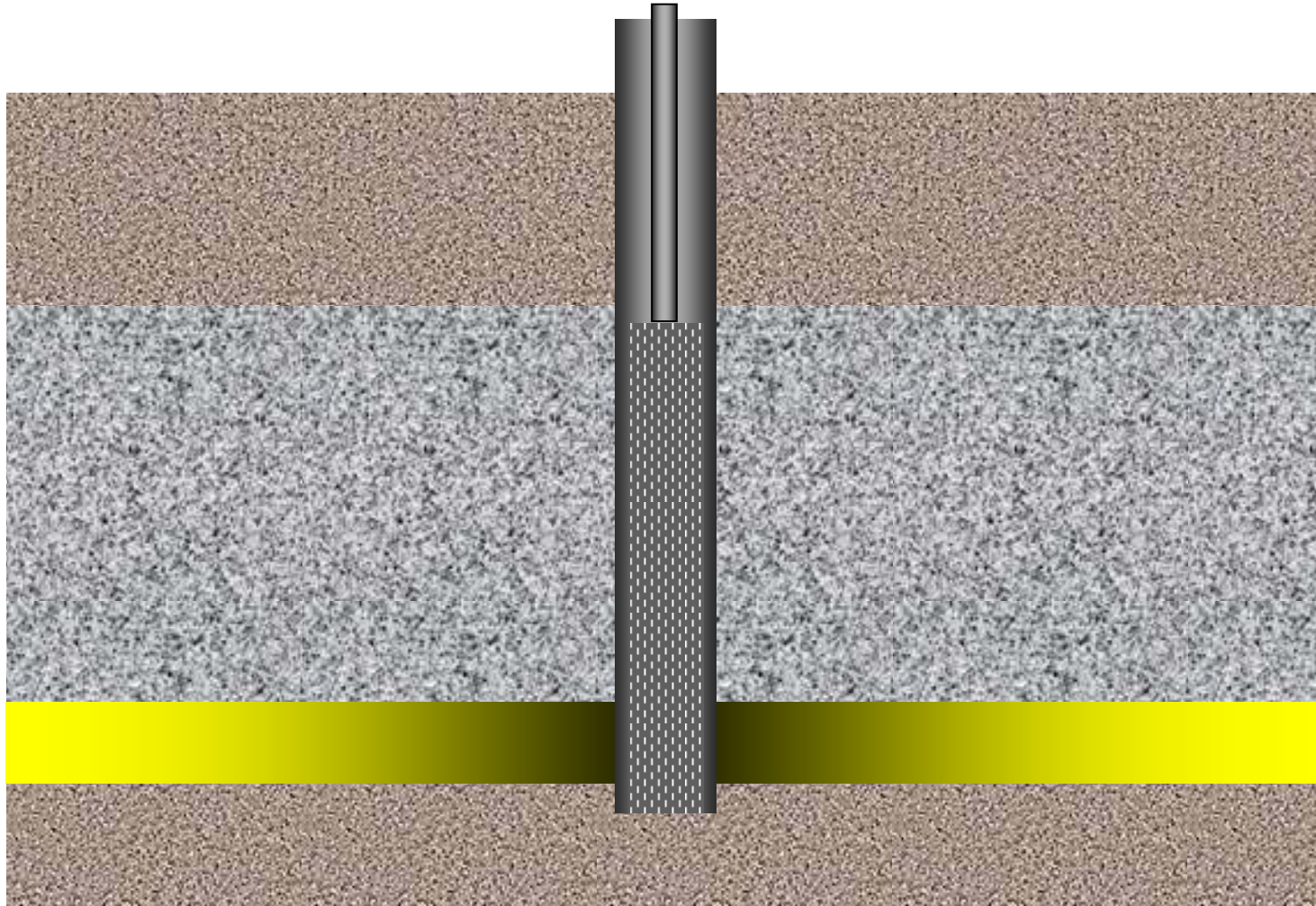
- Hydrate formation prevention :
 - Low FBHP
 - Heat and/or chemical injection
- Freezing:
 - Geothermal < 32 F
 - Heat and/or chemical injection
- Water production
- Others:
 - No significant corrosion
 - No condensate liquids
 - No significant scaling

- Gas hydrate wells will have a relatively benign operating environment – long life and few interventions
- Technologies required to produce gas hydrate wells are currently used in conventional gas field operations
- Capital & operating cost impacts:
 - Compression requirement for gas hydrate wells represents additional costs compared to conventional gas wells
 - Artificial lift requirement and water disposal for gas hydrate wells represent additional costs compared to conventional gas wells
 - Must consider the above in context of field life and reserves recovery per well

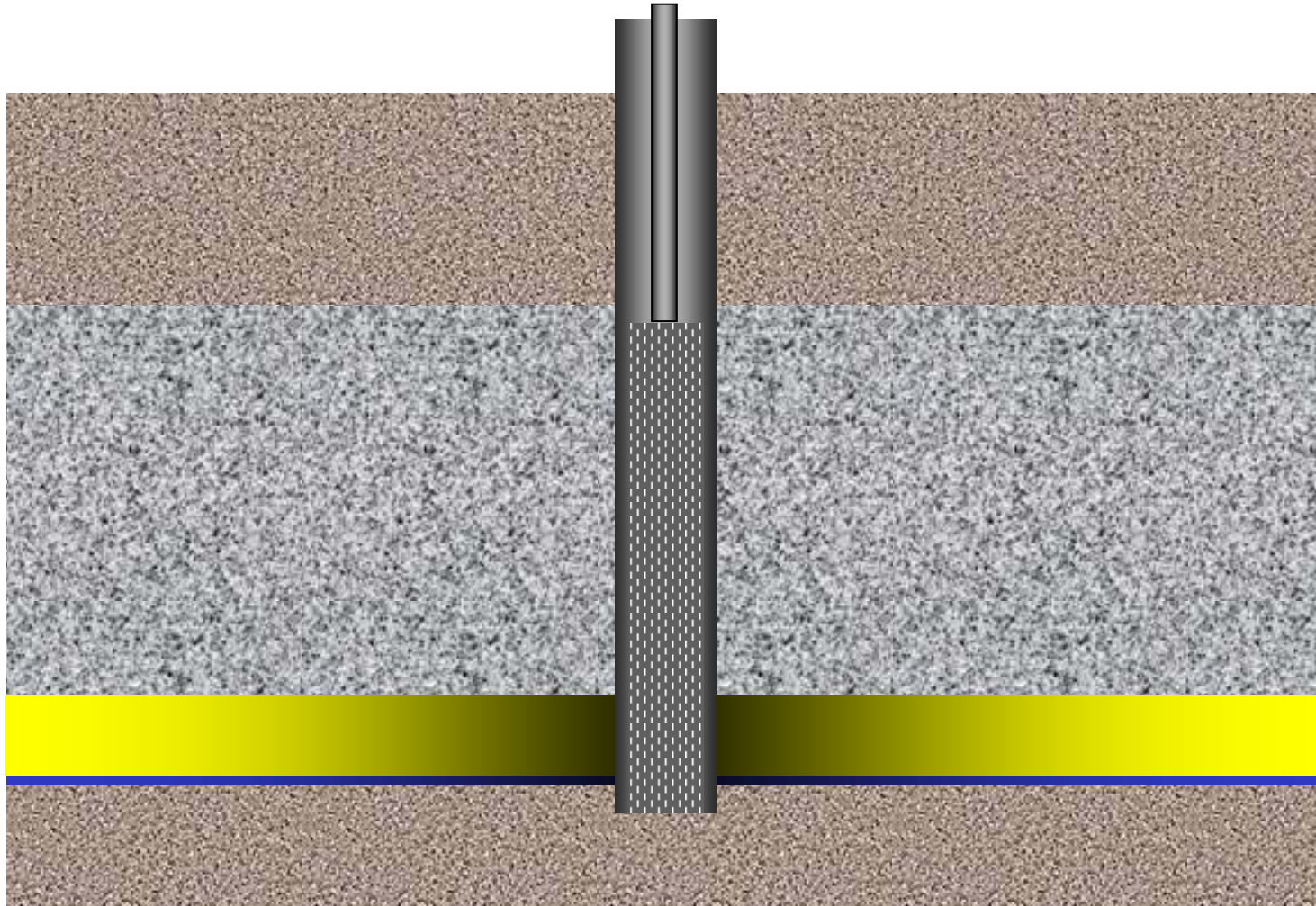
Mallik 5L-38 Hydrate Deposit



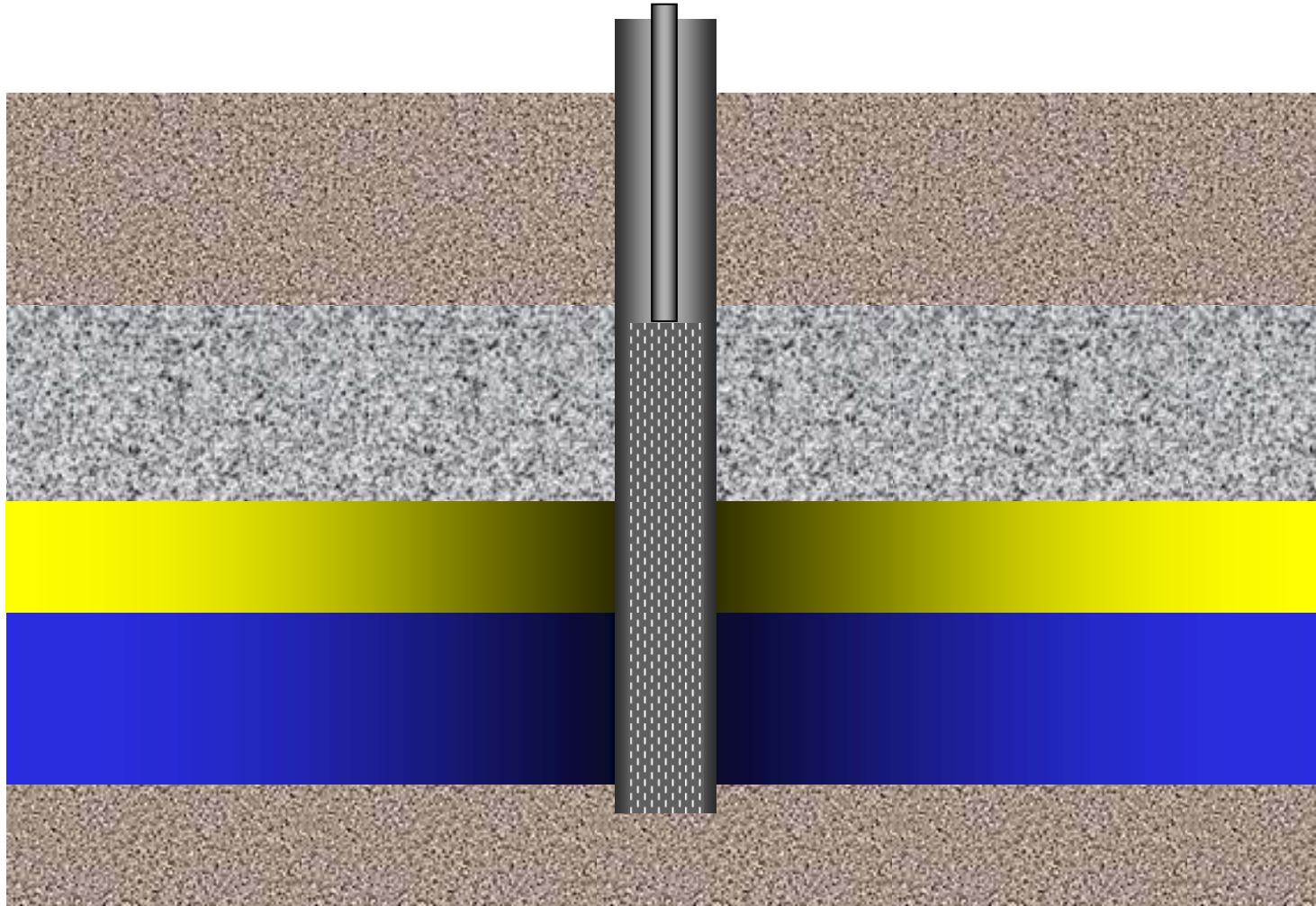
Case 1 – Gas Hydrate Over Free Gas



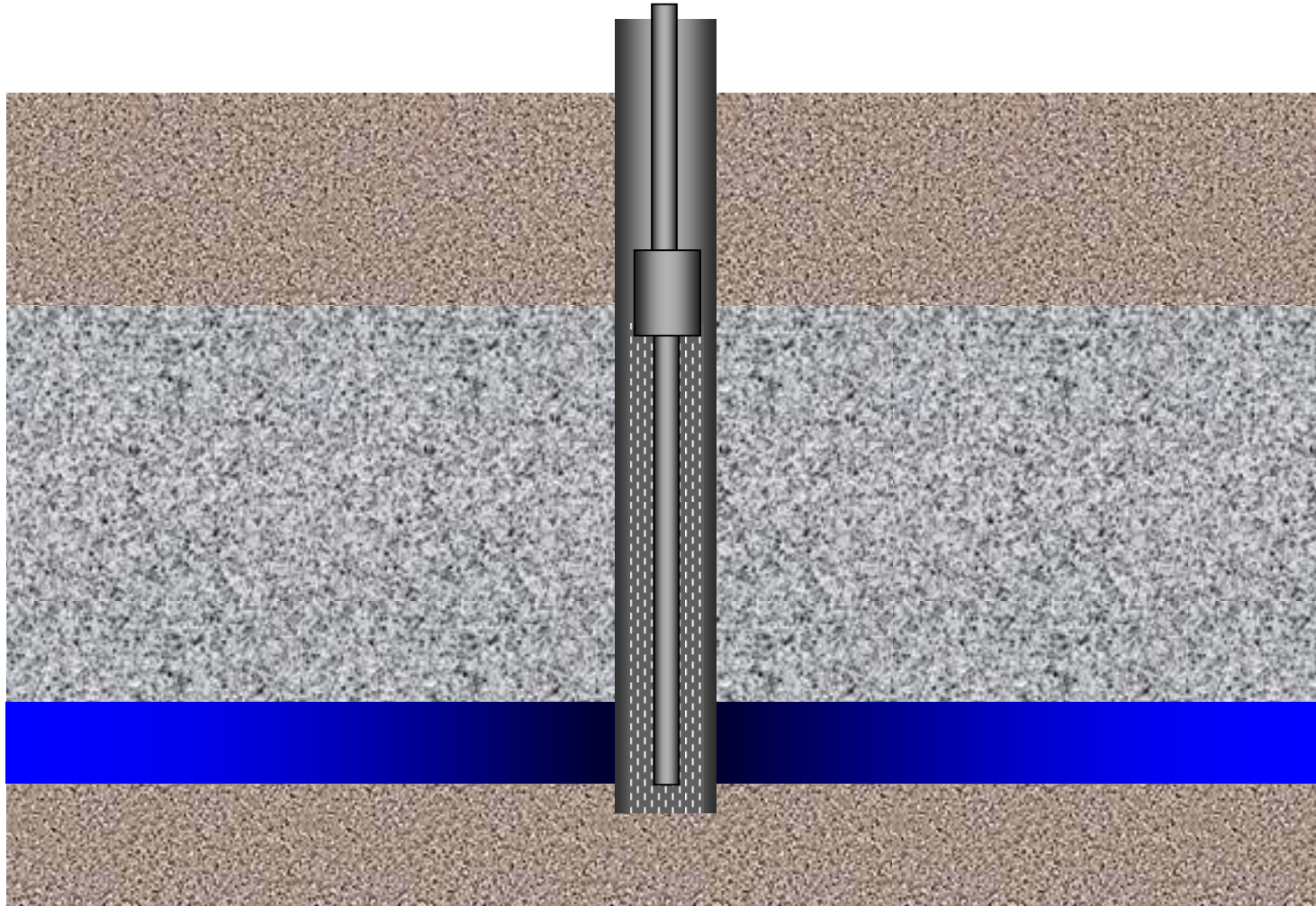
Case 1 – Free Water Established



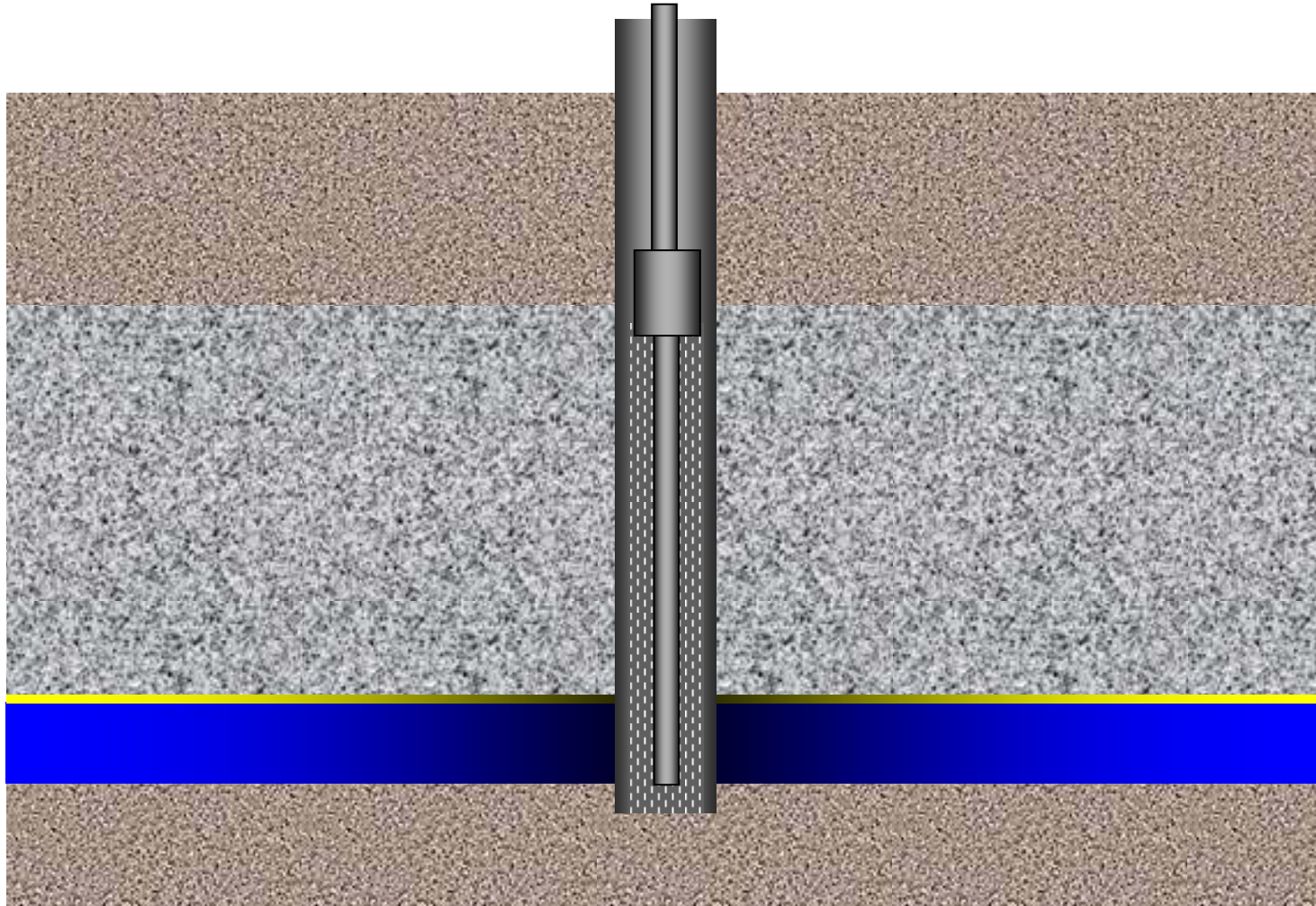
Case 1 – Cont'd Gas Hydrate Dissociation



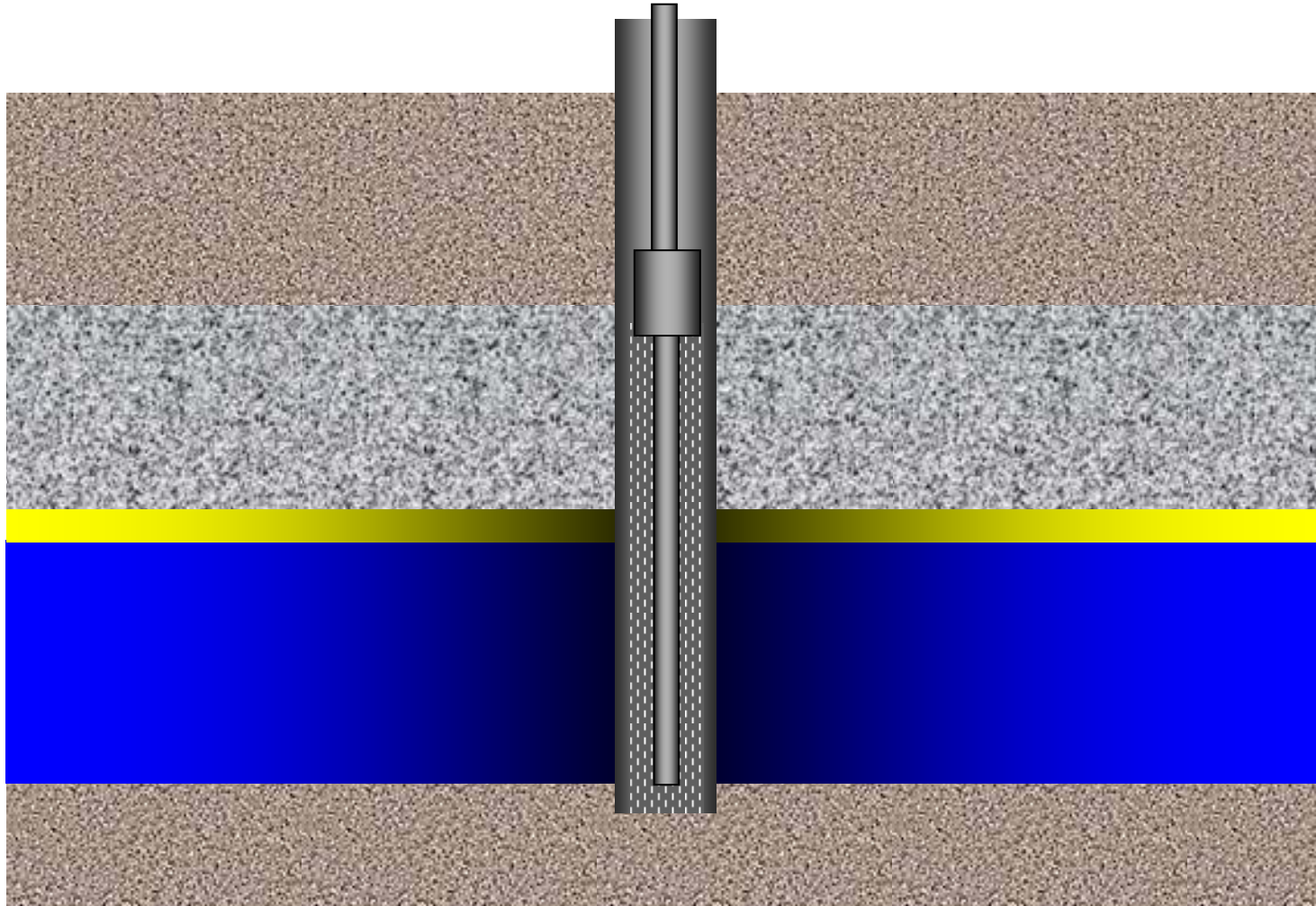
Case 2 – Gas Hydrate Over Water

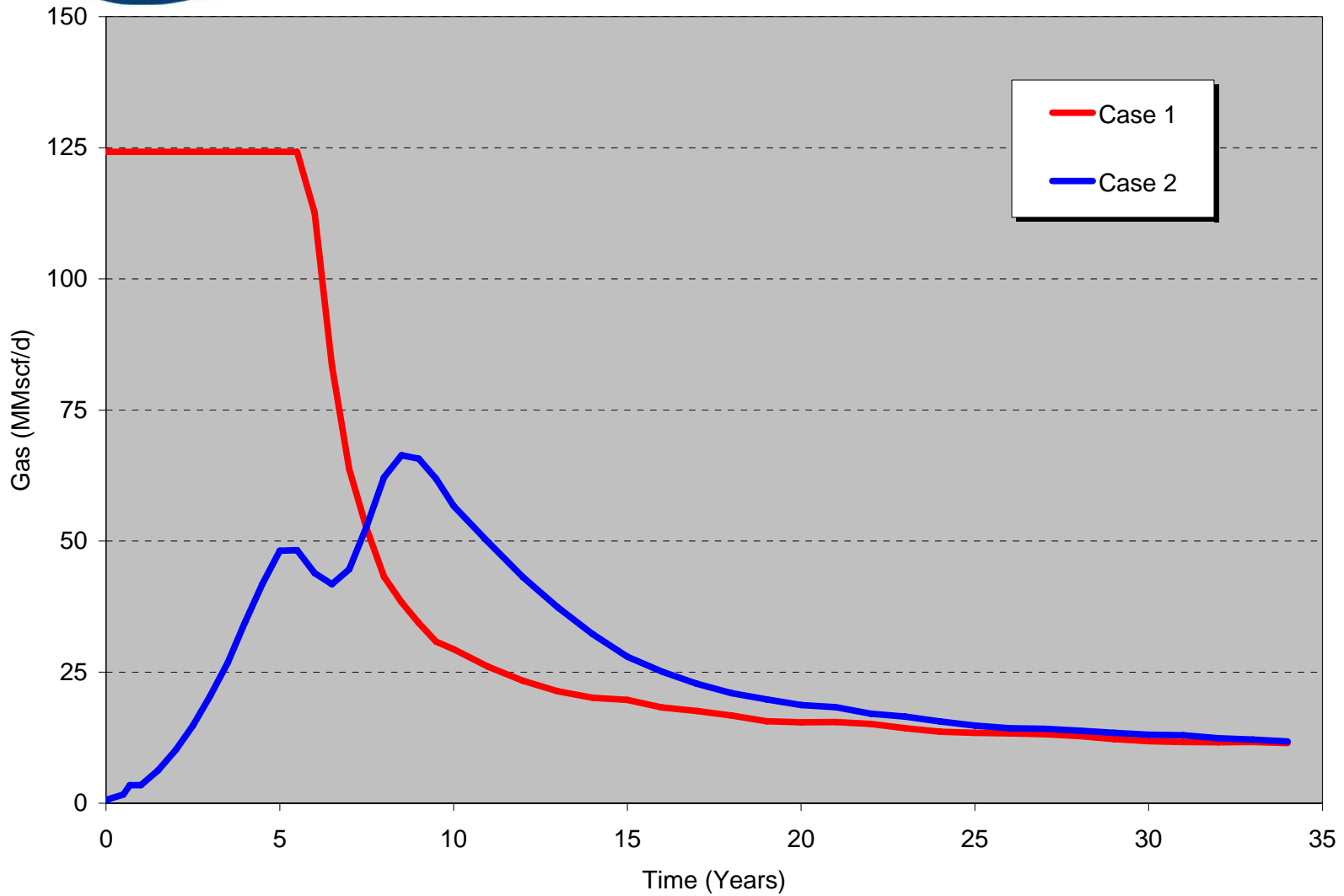


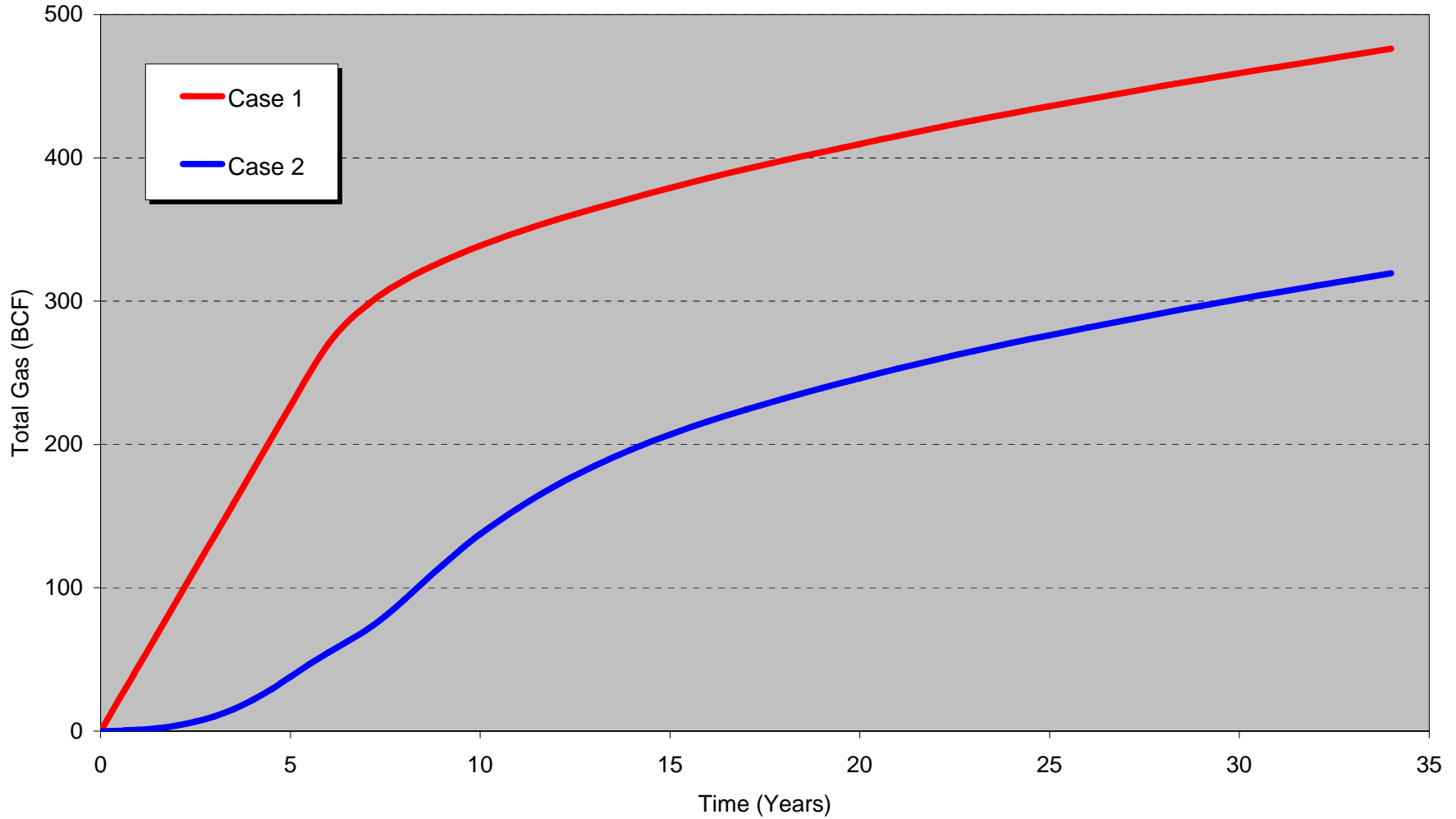
Case 2 – Onset of Gas Production

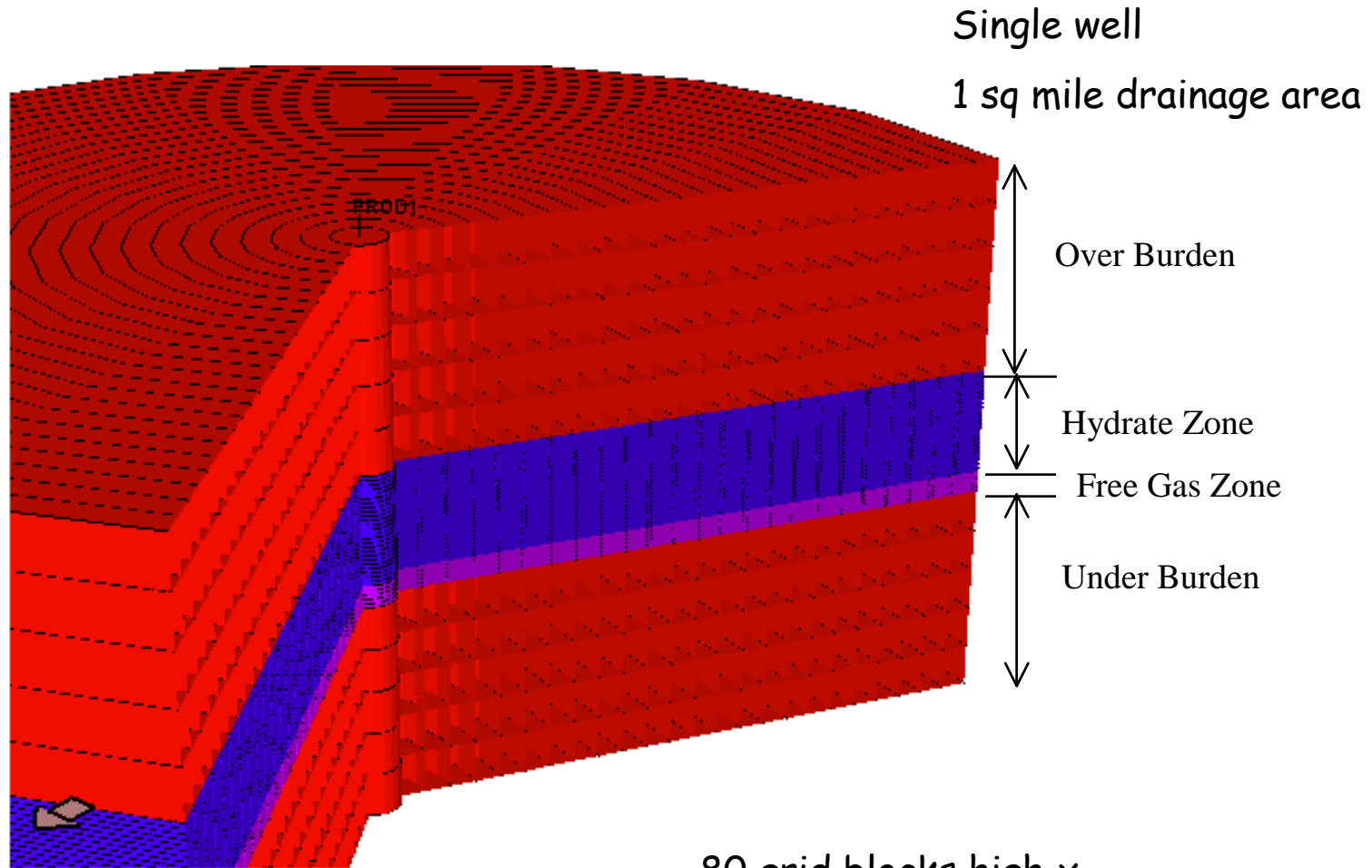


Case 2 – Continued Hydrate Dissociation



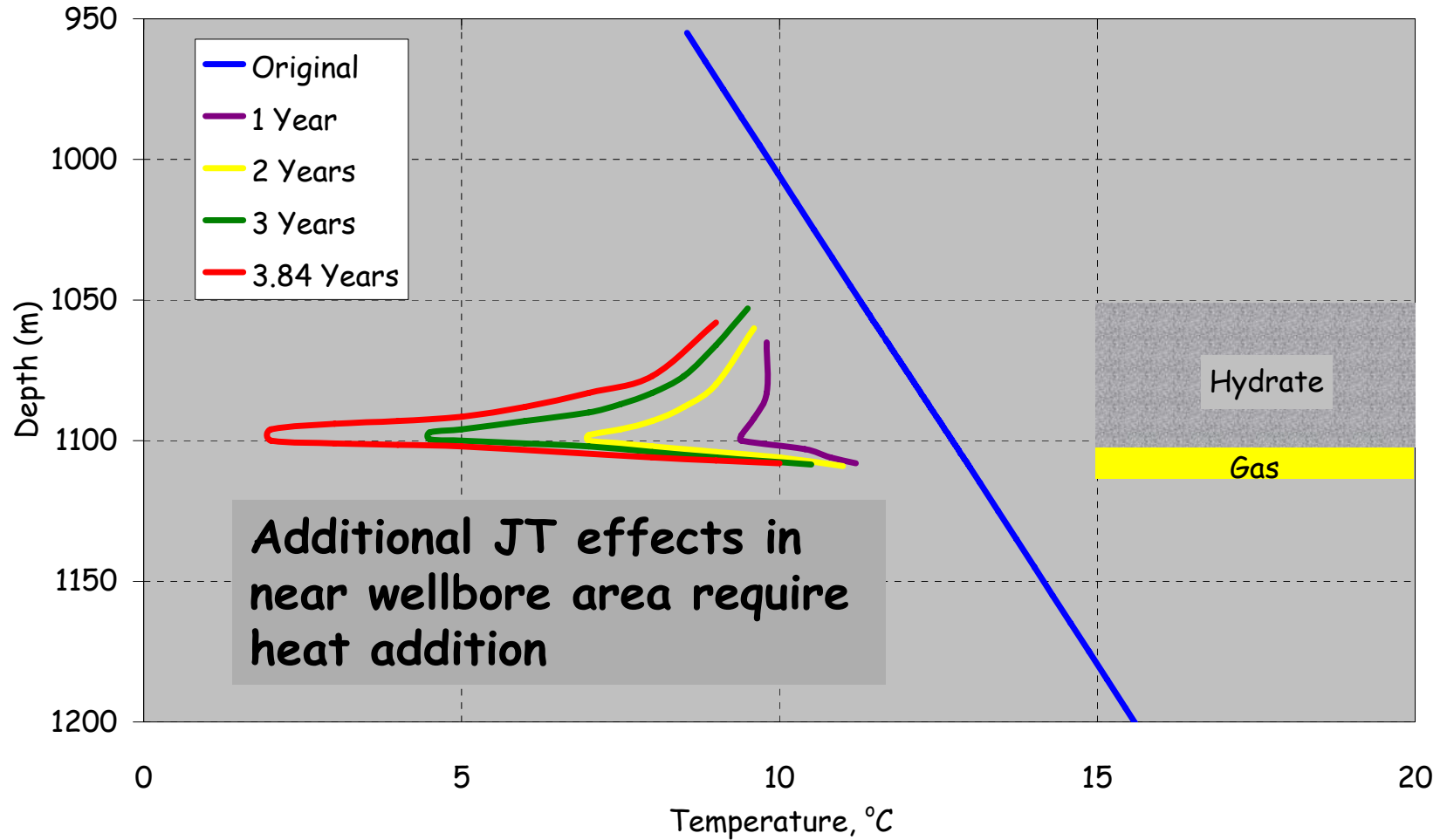






80 grid blocks high x
100 grid block radial

TOUGH-Fx/Hydrate Temperature Profile





Cost Summary - \$CDN 2004 MM

5 Wells, ~1 TCF GIP

Capital Costs	Case 1	Case 2
Drilling & Completions	\$82	\$87
Facilities & Pipeline	\$288	\$198
Sub-total	\$370	\$285
Operating Costs		
Operating Costs	Case 1	Case 2
Local Pipeline	\$18	\$18
Local Facilities	\$374	\$339
Gas Plant Process	\$648	\$431
Water Handling	\$2	\$26
Workovers	\$13	\$18
Pipeline Tariff	\$1,512	\$1,006
Sub-total	\$2,567	\$1,838
Total Capital & Operating	\$2,937	\$2,123



Economic Evaluation - Unit Technical Cost

		Case 1	Case 2
Total Capital & Operating, \$ MM		\$2,937	\$2,123
Sales Gas, BCF		432.1	287.5
\$CDN/Mscf	0% Discount	\$6.80	\$7.39
	10% Discount	\$6.20	\$8.01
	20% Discount	\$5.78	\$9.64